A new approach for flow-through respirometry measurements in humans

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Melanson EL, Ingebrigtsen JP, Bergouignan A, Ohkawara K, Kohrt WM, Lighton JRB. A new approach for flow-through respirometry measurements in humans. Am J Physiol Regul Integr Comp Physiol 298: R1571–R1579, 2010. First published March 3, 2010; doi:10.1152/ajpregu.00055.2010.—Indirect whole room calorimetry is commonly used in studies of human metabolism. These calorimeters can be configured as either push or pull systems. A major obstacle to accurately calculating gas exchange rates in a pull system is that the excurrent flow rate is increased above the incumbent flow rate, because the organism produces water vapor, which also dilutes the concentrations of respiratory gases in the excurrent sample. A common approach to this problem is to dry the excurrent gas prior to measurement, but if drying is incomplete, large errors in the calculated oxygen consumption will result. The other major potential source of error is fluctuations in the concentration of O2 and CO2 in the incumbent airstream. We describe a novel approach to measuring gas exchange using a pull-type whole room indirect calorimeter. Relative humidity and temperature of the incumbent and excurrent airstreams are measured continuously using high-precision, relative humidity and temperature sensors, permitting accurate measurement of water vapor pressure. The excurrent flow rates are then adjusted to eliminate the flow contribution from water vapor, and respiratory gas concentrations are adjusted to eliminate the effect of water vapor dilution. In addition, a novel switching approach is used that permits constant, uninterrupted measurement of the excurrent airstream while allowing frequent measurements of the excurrent airstream. To demonstrate the accuracy of this approach, we present the results of validation trials compared with our existing system and metabolic carts, as well as the results of standard propane combustion tests.

indirect calorimetry; oxygen consumption; human energy expenditure; substrate oxidation

INDIRECT CALORIMETRY IS THE MEASUREMENT OF RESPIRATORY GAS EXCHANGE [E.G., OXYGEN CONSUMPTION (VO2) AND CARBON DIOXIDE PRODUCTION (VCO2)] TO DETERMINE THE METABOLIC RATE OF AN ORGANISM. VO2 AND VCO2 ARE USED TO CALCULATE THE RESPIRATORY QUOTIENT (RQ = VCO2/VO2), WHICH PROVIDES A RELATIVE MEASUREMENT OF FAT AND CARBOHYDRATE OXIDATION. INDIRECT CALORIMETERS TYPICALLY USE FLOW-THROUGH RESPIROMETRY TO MEASURE THE AMOUNT OF A GIVEN GAS PRODUCED OR CONSUMED BY THE ORGANISM. FLOW-THROUGH RESPIROMETRY IS BASED ON THE PRINCIPLE THAT THE AMOUNT OF GAS PRODUCED OR CONSUMED BY AN ORGANISM CAN BE CALCULATED FROM THE CONCENTRATIONS OF THE GASES IN THE INCUMBENT AND EXCURRENT AIRSTREAMS AND THE ASSOCIATED FLOW RATES. FOR EXAMPLE, THE EQUATION TO CALCULATE VO2 USING FLOW-THROUGH RESPIROMETRY IS VO2 = FRi(FO2i) − FRE(FO2e), WHERE FRi AND FRE ARE THE FLOW RATES OF THE INCUMBENT AND EXCURRENT AIRSTREAMS, AND FO2i AND FO2e ARE THE FRACTIONAL CONCENTRATIONS OF OXYGEN IN THE INCUMBENT AND EXCURRENT AIRSTREAMS. FR E NONECESSARILY EQUAL FRE, AND UNDERSTANDING THIS INEQUALITY HAS IMPORTANT IMPLICATIONS FOR UNDERSTANDING THE POTENTIAL SOURCES OF ERROR IN FLOW-THROUGH RESPIROMETRY CALCULATIONS.

The earliest human flow-through calorimeters (respiration chambers) were developed by Pettenkofer (14) and Atwater and colleagues (1, 2). Since then, many other systems have been developed (6, 7, 9, 12, 13, 15–17, 20) and have been used to study human physiology. Most systems in use today can be broadly classified as either push (e.g., air is pushed through the respirometry chamber at a known flow rate) or pull (air is pulled through the respirometry chamber at a known flow rate) systems. Most room calorimetry systems in operation today, particularly in the United States, are pull-type systems (9, 13, 20), although a notable exception is the calorimeter located at Baylor College of Medicine (12), which is a hybrid push-pull closed circuit system, i.e., a pull system with a controlled, minimal, inward pressure gradient. A major obstacle to the accurate calculation of gas exchange rates in a pull system is that excurrent flow rates are increased above the incumbent flow rate (FIO2), because the organism produces water vapor and CO2; the added partial pressures of CO2 and water vapor increase the total pressure, and therefore flow rate of the excurrent airstream. At the same time, CO2 produced by the organism reduces the partial pressure of O2 (i.e., because CO2 is added to the excurrent air, the fractional concentration of O2 in the excurrent air will be reduced). All of these factors must be accounted for in the gas calculations. Although accurately measuring CO2 is not difficult, obtaining an accurate measurement of water vapor pressure so that its dilution effect can be corrected can be challenging. To circumvent this problem, most room calorimetry systems use a gas drying system to reduce water vapor in the excurrent air sample prior to analysis (12, 13, 20). However, if the sample is not completely dry, the measured oxygen concentration will be artificially low because of the dilution effect of water vapor pressure. Importantly, because most systems do not monitor whether water vapor has been completely removed from the airstream, errors can go undetected.

Aside from the problems associated with the dilution effect of water vapor pressure, room calorimeters are prone to two other major sources of error. The first, and generally larger, source of error, particularly with oxygen analyzers, is analyzer drift. Differential gas analyzers reduce, but do not eliminate, drift. Correcting for drift requires periodic recalibration of the analyzer to a standard gas (i.e., baseline) or the excurrent air (8). The latter can be used to monitor drift of the oxygen analyzer because O2 concentrations in the atmosphere are quite

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stable after adjusting for the variable gas components (water vapor and CO₂). Thus, it is usually reasonable to assume that the fractional concentration of dry, CO₂-free incurrent air is 0.2094 (11, 21), and analyzer drift can be corrected on this basis. In the case of CO₂, analyzer drift is less of a problem, but accuracy is affected by the second source of error, which is variability in the CO₂ concentration of the incurrent air (e.g., due to pollution, traffic levels, day/night cycles, and other environmental influences). Ideally, the gas concentrations in the incurrent airstreams should be periodically measured. Correcting either of the above sources of error requires switching the analyzer chains between the incurrent and excurrent airstreams. This introduces discontinuities in the metabolic data, which may explain why this approach is not commonly used. Most calorimeters are operated under the assumption that the concentrations of O₂ and CO₂ in the incurrent airstream are constant and do not adjust for analyzer drift or variability in FICO₂.

We operated a pull-type room calorimeter at the University of Colorado Denver from 1993 to 2006 that was designed after the calorimeters located at the National Institutes of Health Facility in Phoenix, AZ and Vanderbilt University in Nashville, TN (20). The source of incurrent air was recirculated building air, which proved to be very problematic because of variability in the incurrent CO₂ concentration. In 2007, we moved to a new location, and a new pull-type calorimeter was constructed. In this new setup, the problem associated with recycled building air was circumvented by drawing incurrent air directly from the environment. However, this introduced an unanticipated problem related to the unique environmental conditions in Denver (elevation ~5,280 ft), which include consistently low barometric pressures coupled with exceptionally dry ambient air, particularly in the winter months, when dew points are often below ~10°C.

The purpose of this paper is to describe a new flow-through respirometry system (Sable Systems International, Las Vegas, NV) for indirect room calorimetry that minimizes errors related to the incomplete removal of water vapor, analyzer drift, and variability in gas concentrations of incurrent air. To evaluate the accuracy of the Sable Systems flow-through respirometry system (Sable system), we conducted extensive validation trials using a variety of approaches. First, we performed simultaneous, parallel measurements with the new Sable system and the existing system during propane combustion tests when the dew point in the incurrent air was both above and below 0°C. Second, we measured VO₂, VCO₂, energy expenditure (EE), and RQ during several different activities performed in the calorimeter and compared the measurements obtained using both the Sable and the existing systems to those obtained using a metabolic cart. Third, we performed simultaneous, parallel 24-h measurements using the Sable and existing systems. Finally, we tested the dynamic response of the 24-h RQ measurements by studying human subjects under conditions known to induce dramatic changes in RQ (i.e., manipulation of macronutrient intake).

METHODS

Institutional Approval

The human study protocols included in this analysis were approved by the Colorado Multiple Institutional Review Board and the Scientific Advisory Board of the Clinical Translation Research Center (CTRC) at the University of Colorado Denver, Denver CO. All subjects provided informed written consent.

Description of the Room Calorimeter

The calorimeter room measures ~3.6 × 3.3 × 2.4 m (length × width × height), with a total volume of ~28.5 m³. The room is located in the CTRC inpatient unit on the 12th (top) floor of the University of Colorado Hospital. Incurrent air is drawn from the external environment above the building into a storage buffer above the calorimeter. The buffer was intended to ensure stability of the O₂ and CO₂ concentration of the incurrent air, and is kept at a slight positive pressure relative to the surrounding environment. The volume of the buffer is ~20 m³ (~1.1 × 3.2 × 5.8 m³). Temperature of the air in the buffer is controlled at 23.9°C, but is not otherwise conditioned. Temperature (22.0 ± 1.0°C) and relative humidity (30–50%) inside the calorimeter room are controlled using a ceiling-mounted fan coil unit (model TSC-08; McQuay International, Minneapolis, MN) (Fig. 1). The fan coil unit is also used to perform mixing of the air within the room; airflow within the room is recirculated at a rate of ~20 m³/min. At this rate, the volume of air inside the calorimeter is mixed approximately every 2 min, which ensures fast response time for the measurement of VO₂ and VCO₂. Temperature, barometric pressure, and relative humidity inside the room are measured continuously using a dew point hygrometer (General Eastern Optica Dewpoint Meter; GE Infrastructure Sensing, Billerica, MA). Technical specifications and descriptions of the Sable and existing systems are contained in the APPENDIX.

Fig. 1. The room calorimeter located at the University of Colorado Denver. The fan coil unit is indicated by the solid arrow. The pipes in the spider configuration on the ceiling are the sampling ports.
Validation of the accuracy in measuring $\dot{V}O_2$, $\dot{V}CO_2$, EE, and RQ is routinely performed based on the recovery of O2 and CO2 while propane is burned. We expect all variables to be $\geq 98\%$ of anticipated values. We performed simultaneous propane tests with both the Sable and the existing systems when the dew point was both above and below 1°C to demonstrate the effect of ineffective drying and the dilution effect of water vapor pressure.

Validation against metabolic cart. $\dot{V}O_2$, $\dot{V}CO_2$, EE, and RQ were measured during three different activities (resting, bench stepping, stationary cycling) using a metabolic cart (TrueOne 2400; Parvo-Medics, Sandy, UT). Measurements were obtained on six individuals (2 male, 4 females). Subjects arrived in the CTRC at 7:30 AM following an overnight fast and having abstained from strenuous exercise for at least 24 h.

RESULTS

All values are means ± SE, unless otherwise specified.

Table 1. Results of propane test with positive and negative ambient dew points

<table>
<thead>
<tr>
<th></th>
<th>Positive Dew Point</th>
<th>Negative Dew Point</th>
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</thead>
<tbody>
<tr>
<td></td>
<td>Expected</td>
<td>Existing System</td>
</tr>
<tr>
<td>$\dot{V}O_2$, liters</td>
<td>374.4</td>
<td>372.1 (99.4)</td>
</tr>
<tr>
<td>$\dot{V}CO_2$, liters</td>
<td>224.6</td>
<td>228.0 (101.4)</td>
</tr>
<tr>
<td>EE, kcal</td>
<td>1,724.0</td>
<td>1,718.5 (99.7)</td>
</tr>
<tr>
<td>RQ</td>
<td>0.6000</td>
<td>0.6130 (102.2)</td>
</tr>
</tbody>
</table>

During the positive dew point test, 147 g of propane was combusted over 1,168 min (±0.13 g/min), and during the negative dew point test, 126 g was combusted over 827 min (±0.15 g/min). Numbers in parentheses indicate %expected. $\dot{V}O_2$, oxygen consumption; $\dot{V}CO_2$, carbon dioxide production; EE, energy expenditure; RQ, respiratory quotient.
98% of expected values with both systems. However, \( \dot{V}O_2 \) was 100% of expected values with the Sable system, but 141% of expected values with the existing system. As a result, the EE calculated with the existing system was 135%, but RQ was only 71%, of the expected value. \( \dot{V}CO_2 \) tracked very closely over the entire measurement period with both systems, but there was an obvious divergence in measured \( \dot{V}O_2 \) and RQ. Validation with the Metabolic Cart

At rest and during stepping and cycling, \( \dot{V}O_2 \), \( \dot{V}CO_2 \), EE, and RQ measured by the metabolic cart did not differ with measurements obtained by either of the room calorimeter systems (Fig. 3). It is interesting to note the RQ response. RQ is lowest during resting activities (reflecting a higher use of fat as a substrate) but increases during even light activities, such as stepping, and will further increase with increasing exercise intensity. Increases in RQ from rest to stepping and then cycling were only detected with the Sable system. Over the entire 4-h measurement period, \( \dot{V}O_2 \) measured by the existing calorimeter was significantly higher than that measured by the Sable system (Table 2). However, the magnitude of this difference was small (~5 liters), and the measurements were significantly correlated. Likewise, total EE measured by the existing system was significantly higher than with the Sable system (average difference ~17 kcal), but the measurements were highly correlated. In contrast, \( \dot{V}CO_2 \) measured by the existing system was significantly lower than that measured by the Sable system, but again the magnitude of difference was small (~2 liters) and the measurements were highly correlated. The correlation between the existing and Sable systems for RQ was \( r = 0.89 \).

24-h Comparisons

Similar to the 4-h tests, 24-h \( \dot{V}O_2 \) and EE measured by the existing system was significantly higher than that measured by the Sable system (Table 3). However, the magnitude of the differences were small (~15 liters, 60 kcal), and the measurements were highly correlated (Fig. 4). There were no differences in total \( \dot{V}CO_2 \). As in the 4-h tests, 24-h RQ was ~ 0.03 higher (\( P < 0.01 \)) with the Sable system. The correlation for RQ between the two systems was \( r = 0.54 \). A sample 24-h measurement in a single subject (Fig. 5) demonstrates the level of agreement between the two systems.

Response of 24-h RQ

When fed the low-fat diet, 24-h RQ for the first subject (S1) was close to the food quotient of the diet, as measured by each system (Fig. 6). When fed the high-fat diet, 24-h RQ decreased close to the food quotient of the diet, and similar values were
RESULTS

In this report, we describe the accuracy of a new approach to performing whole room indirect calorimetry. This new approach incorporates two novel aspects of operation: 1) constant measurement of water vapor pressure in the incurrent and excurrent airstreams, permitting the accurate adjustment of the measured \( \dot{V}_{O_2} \) for the dilution effect of water vapor pressure, which eliminates the need of drying the gasses; and 2) implementation of a new switching approach that permits constant, uninterrupted measurement of the excurrent airstream, while allowing frequent measurements of the incurrent airstream, and that allows for continuous and dynamic adjustments to the incurrent gas concentrations due to both changes in gas concentrations in the incurrent air and analyzer drift. To determine the accuracy of this new approach, we performed several different validation studies. Using propane combustion, the constant standard for validating the performance of a room calorimeter, we demonstrated that recovery of \( O_2 \) and \( CO_2 \) were within 2% of expected values. We also demonstrated that under conditions where water vapor pressure is not removed from the incurrent airstream (i.e., the dew point is <1°C), recovery of \( O_2 \) and \( CO_2 \) were still >98%. In fact, the Sable system consistently yields recoveries for both \( O_2 \) and \( CO_2 \) that are greater than ~98% of expected values (Table 1). Next, we compared \( \dot{V}_{O_2} \), \( \dot{V}_{CO_2} \), RQ, and EE measured at rest and during physical activity against that measured using a metabolic cart. Results of this study showed good agreement between the metabolic cart and the Sable system. We also compared 4-h continuous measurements obtained with our existing system and the Sable system. Although there were significant differences in \( \dot{V}_{O_2} \) and EE, the magnitude of these differences was relatively small.

DISCUSSION

Table 2. Calorimeter results at 4 h

<table>
<thead>
<tr>
<th></th>
<th>Existing System</th>
<th>Sable System</th>
<th>( P )</th>
<th>( r )</th>
</tr>
</thead>
<tbody>
<tr>
<td>( \dot{V}_{O_2} ), liters</td>
<td>110.6 ± 22.6</td>
<td>105.4 ± 20.4</td>
<td>&lt;0.01</td>
<td>0.99</td>
</tr>
<tr>
<td>( \dot{V}_{CO_2} ), liters</td>
<td>92.6 ± 18.0</td>
<td>95.5 ± 18.6</td>
<td>0.47</td>
<td>0.99</td>
</tr>
<tr>
<td>EE, kcal</td>
<td>538.0 ± 109.4</td>
<td>520.9 ± 100.6</td>
<td>0.05</td>
<td>0.99</td>
</tr>
<tr>
<td>RQ</td>
<td>0.84 ± 0.05</td>
<td>0.87 ± 0.04</td>
<td>0.01</td>
<td>0.89</td>
</tr>
</tbody>
</table>

Values are means ± SD.

obtained for each system. The 24-h EE measured by the existing system was 2,145 and 2,197 kcal/day for the low-fat and high-fat diets, respectively, and 2,060 and 2,105, respectively, when measured by the Sable system. For the second subject (S2), the 24-h RQ measured by each system was below the food quotient of the low-fat diet, but similar between systems. When fed the high-fat diet, 24-h RQ decreased as expected. Unexpectedly, the dew point was negative on this day. As a result, \( \dot{V}_{O_2} \) measured by the existing system (732 liters) was substantially higher than that measured by the Sable system (495 liters), although there was close agreement in the measured \( \dot{V}_{CO_2} \) (395 and 389 liters, respectively). Thus, once again, we demonstrate that when the incurrent airstream is not completely dried and the dilution effect of water vapor pressure on the partial pressure of \( O_2 \) is not accounted for, the resulting calculated \( \dot{V}_{O_2} \) will be too high (and RQ will be too low).

Table 3. Calorimeter results at 24 h

<table>
<thead>
<tr>
<th></th>
<th>Existing System</th>
<th>Sable System</th>
<th>( P )</th>
<th>( r )</th>
</tr>
</thead>
<tbody>
<tr>
<td>( \dot{V}_{O_2} ), liters</td>
<td>434.5 ± 83.7</td>
<td>418.8 ± 85.7</td>
<td>&lt;0.01</td>
<td>0.99</td>
</tr>
<tr>
<td>( \dot{V}_{CO_2} ), liters</td>
<td>362.1 ± 73.2</td>
<td>363.6 ± 71.3</td>
<td>0.47</td>
<td>0.99</td>
</tr>
<tr>
<td>EE, kcal</td>
<td>2,112.9 ± 409.4</td>
<td>2,052.7 ± 414.5</td>
<td>&lt;0.01</td>
<td>0.99</td>
</tr>
<tr>
<td>RQ</td>
<td>0.83 ± 0.04</td>
<td>0.86 ± 0.05</td>
<td>0.01</td>
<td>0.69</td>
</tr>
</tbody>
</table>

Values are means ± SD.

As described in the INTRODUCTION, the environmental conditions in Denver (dry air coupled with constantly low barometric pressure) create a unique set of challenges for implementing a pull-type indirect calorimetry. Although our choice to use environmental air as a source of reference gas for the differential analyzers eliminated one source of error (i.e., potentially large fluctuations in concentrations of \( O_2 \) and \( CO_2 \) in the incurrent air), it introduced a new, unanticipated source of error (i.e., low dew point in the incurrent air, particularly during the winter months). Because we employed a chilled water cooler, which can only chill the sample gasses to 1°C, to dry both the incurrent and excurrent airstreams, this introduces an error into the measurement of \( \dot{V}_{O_2} \). Although the dew point of the incurrent airstream is periodically <1°C, the dew point of the incurrent airstream will always be positive (because the subject is respiring, water vapor is added to the excurrent air). Under this situation, the chilled water cooler will dry the gas in the excurrent air, but not the incurrent air, thus inducing an error in the calculated \( \dot{V}_{O_2} \) because the dilution effect of water vapor pressure on \( O_2 \) in the incurrent air was not considered in the calculations. The Sable system circumvents this problem, and the need for drying, by constantly measuring and adjusting for the dilution effect of water vapor pressure on \( O_2 \) and \( CO_2 \). Importantly, even small fluctuations in the difference in water vapor pressure in the incurrent and excurrent air can introduce
substantial errors in the measured \(\text{O}_2\) concentrations. Thus, if unequal drying occurred in the two samples (incurrent and excurrent), a potentially large and undetected error could occur. Thus, the continued use of this type of drying system in room calorimeters is questioned.

Prior to installing the Sable system, we explored several alternative approaches for drying the gasses. One possibility was to use a desiccant column; a commonly used column is calcium sulfate (gypsum). However, a characteristic of gypsum is that it absorbs \(\text{CO}_2\), and would therefore introduce another source of error in the metabolic calculations. We also considered the use of a counterflow approach, as used in the calorimeters in Department of Human Biology, Maastricht University, Maastricht, The Netherlands (15). This approach uses a specialized drying tube that has a center tube surrounded by a membrane that permits exchange of water vapor. The center tube is surrounded by an outer tube, and a dry gas (e.g., 100% oxygen or nitrogen) flows through the outer tube in a direction counter to the flow of the sample gas. However, supplying a source of continuous gas is expensive; it requires a source of dry gas be delivered via central lines in the building to the calorimeter, or tanks of gas that are replaced on a regular basis.

Prior to installing the Sable system, we circumvented the problem induced when the dew point of the incurrent air was \(-10^\circ\text{C}\) by installing water baths upstream from the chilled water cooler. The samples from both the incurrent and excurrent airstreams were passed through small flasks that were filled to \(-75\%\) with water (the gasses passed through the airspace above the water). In this manner, the samples would be moistened and would therefore raise the dew point of both samples above \(0^\circ\text{C}\). Although we did not measure the dew point to confirm this, we conducted numerous propane tests when the dew point was \(-10^\circ\text{C}\); the result was that recovery of \(\text{O}_2\) was restored to \(-98\%\) (data not shown). However, we were aware that this was not an ideal setup; because \(\text{CO}_2\) is highly soluble in water, this probably induced a lag in \(\text{CO}_2\) response time. Although 24-h recoveries of \(\text{CO}_2\) during the propane tests were also \(-98\%\), we were skeptical of \(\text{CO}_2\) measurements over short periods of time. Thus, we deemed this approach unacceptable, which ultimately led us to consider the Sable system.

Another novel aspect of the Sable system is the use of fuel cell oxygen sensors to measure the fractional concentrations of \(\text{O}_2\). Paramagnetic oxygen analyzers are highly accurate, with a very short response time and high resolution, and their use in room calorimetry is well established. Fuel cell oxygen analyzers have only recently attained the level of resolution of paramagnetic analyzers; however, they are continuing to improve. Because fuel cell oxygen analyzers are electrochemical in nature, they have the potential to yield signals with less noise than paramagnetic oxygen analyzers, which use various complex systems that transduce the forces exerted by oxygen concentration differences within inhomogeneous magnetic fields. For example,
using the same dual-absolute fuel cell oxygen analyzer we used in this study, atmospheric scientists have attained a resolution of 0.3 ppm O₂ against a background of atmospheric air (19). On the other hand, the response times of fuel cell oxygen analyzers are significantly slower than those of paramagnetic oxygen analyzers (~7 s vs. 0.2 s). However, in the case of room calorimetry, or indeed in most forms of flow-through respirometry, response times are primarily determined by the time constant of the respirometry chamber (volume/flow rate), which is usually in the range of minutes to (in the case of room calorimetry) hours. Most time-response correction algorithms for room calorimeters employ the first derivative of the gas analyzer signals and are thus extremely sensitive to analyzer noise. Under these circumstances, analyzer noise is a more important determinant of overall system performance than analyzer response time.

In addition to solving the problem with inadequate drying of the sample gasses, we have observed several other advantages to operating the Sable system. First, eliminating the drying step eliminates a need for regular maintenance of the chilled water cooler; the peristaltic pumps that remove the condensed water needed to be replaced approximately every 12–18 mo. It is likely that other drying systems require periodic maintenance as well. Second, because the Sable system continuously baselines the gas analyzers, there is no need for daily calibration of the gas analyzers, which can be a time-consuming process (as well as another source of potential error). Finally, since the Sable system is an integrated system specifically designed for the purpose of measuring metabolism in flow-through respirometers, it is very user friendly. Our experience with our previous systems and knowledge of other room calorimeters is that these systems have been developed with “off the shelf” components and often employ user-written customized software.

Perspectives and Significance

We have demonstrated the validity of a new approach to measuring gas exchange in humans using whole room indirect calorimetry. The novel aspects of this approach are the continuous measurement of relative humidity and temperature, permitting the accurate and continuous calculation of water vapor pressure and frequent measurement of incidental gas concentrations without interrupting the measurement of the incidental airstream. These features permit continuous adjustment for the dilution effect of water vapor pressure and changes in the background concentrations of O₂ and CO₂, thus accounting for the two major sources of error in pulley-type room calorimeters.

APPENDIX

Description of the Room Calorimeter

The calorimeter has an external window and is furnished with a hospital bed, desk, chair, flat-screen, wall-mounted television, computer with internet connection, telephone, and a sink and toilet. Two air-locking passages are mounted in the wall and are used to pass meals to the subject and collect biological specimens (e.g., urine samples) with minimal disturbance of the internal environment of the room. A blood sampling port is also mounted in the wall of the calorimeter; when the covers are removed, the subject can extend his/her arm through a rubber iris sleeve for blood sampling, again without disturbing the internal environment of the room. A video camera is mounted in the corner of the room with video monitors located in the calorimeter control room and at the nursing station. The calorimeter is also equipped with an intercom system, which facilitates communication with the research subjects during the study periods.

Description of the Existing Respirometry System

Air is pulled from the room at a constant rate of 80 l/min and replaced with fresh air from the buffer using an adjustable DC-powered fan (Rotron Minispiral Regenerative Blower; Ametek, Paoli, PA). Excurrent flow rate is measured using a mass flow meter (Teledyne Hastings HFM-200 LFE; Teledyne Hastings Instruments, Hampton, VA). The difference in gas concentrations in the incidental and excurrent airstreams is measured using a differential paramagnetic oxygen analyzer (Siemens Oxyomat 6E Oxygen Gas Analyzer; Siemens, Houston, TX) and a differential infrared carbon dioxide analyzer (ABB Advance Optima Urs 14 NDIR CO₂ Analyzer; ABB, Zurich, Switzerland). Span ranges of the O₂ and CO₂ analyzers are 20–21% and 0–1%, respectively. Subsamples of both the incidental and excurrent airstreams are passed through a chilled water gas cooler (ABB Model SCC-C Sample Gas Cooler). The chilled water cooler is placed upstream from the gas analyzers, and samples from both the incidental and excurrent airstreams are chilled to 1°C. This condenses the moisture from the samples and the airstreams are dried to a water vapor pressure corresponding to 1°C, which is ~0.66 kPa or 4.93 Torr. Flow through the cooler is controlled (~1 l/min) by using an ABB model SCC-F Sample Gas Feed Unit that also provides control for the flow rate through the gas analysis chain. The temperature of the chilled water cooler is 1°C, as the gas passes through the cooler, moisture condenses and is removed using peristaltic pumps. The CO₂ and O₂ analyzers are aligned in series. After exiting the CO₂ analyzer, the airstreams are warmed to 37°C by using a water bath to ensure constant temperature of both the incidental and excurrent airstreams entering the O₂ analyzer. Analog data signals are converted to digital using a 16-bit A/D converter (model PCI-DAS1602/16; Measurement Computing). Data are collected at 60 Hz, for 8 s of each minute, and averaged to obtain average minute values. A custom-written program controls data collection, and data are processed using a fast-response algorithm that suppresses noise and identifies trends yielding improved transient response (13). Briefly, this algorithm determines the two connected exponential equations, using the least-squares method, that best fit the previous 30 min of data from the present minute, and calculates the smoothed gas concentration and time derivative from 15 min prior to the present minute. These values are then substituted into the respiration equations, and the process is repeated every minute. The system is calibrated prior to each study visit. Before the subjects enter the calorimeter, the O₂ and CO₂ analyzers are calibrated to a zero value and a span value. During the zero calibration, both channels of the analyzers are fed gas from a tank containing an ambient gas mixture of 20.94% O₂ and 0.3% CO₂, thus the recorded difference between the analyzer channels is 0.0%. During the span calibration, the sample line from the calorimeter is fed a gas mixture containing ~20.1% O₂ and 0.9% CO₂, and the reference line is fed ambient tank gas; thus, the span value differences are ~0.8% for both the O₂ and CO₂ analyzers. Periodically (approximately once a month), the precision of the system is tested using propane combustion tests. A bottle of propane is combusted at a rate of ~0.15 g/min, as determined by serial data recorded from a balance scale (Denver Instrument model FX-1502; Fisher Scientific, Pittsburgh, PA) beneath the bottle, and the expected volume of O₂ and CO₂ is determined based on expected production of 2.55 and 1.53 l of O₂ and CO₂, respectively, per gram of propane burned (22). The total VO₂ and VCO₂ measured by the system are expressed as a percentage of the expected values. Initially, these tests showed that the previous system was substantially in error. The manufacturer-supplied calibration gas concentrations were therefore adjusted by back calculation to yield appropriate propane burn results.
Description of Sable System

The Sable system is designed to minimize errors related to the incomplete removal of water vapor, analyzer drift, and variability in gas concentrations of incumbent air. The primary enhancements are 1) the use of a fuel cell-based oxygen analyzer; 2) high-precision continuous measurement of relative humidity and temperature, permitting the accurate and continuous calculation of water vapor pressure; and 3) frequent measurements of incumbent gas concentrations. The first two enhancements eliminated the need for drying the airstreams and, more importantly, eliminated errors introduced when the dew point of the incumbent air was below 0°C. The third enhancement was accomplished by using a novel switching approach that permits constant, uninterrupted measurement of the incumbent airstream, while allowing frequent measurements of the incumbent airstream.

New hardware and software were installed for the room calorimeter in June 2009 and operated in parallel with the existing system. The Sable system is completely contained (i.e., all analyzers and components manufactured by Sable Systems International). A variable rate (0–500 l/min) mass flow generator (Sable Systems FlowKit-500) pulls the air from the chamber. A subsample of the incumbent airstream (~400 ml/min) is pulled through a flow-switching unit (Sable Systems Background Baselining Unit), using a variable subsampling pump (Sable Systems model SS-4), from which it passes through two complete gas analysis systems that comprise two water vapor-, two carbon dioxide-, and two oxygen-analyzers plus a barometric pressure sensor. For water vapor analysis, two Sable Systems RH-300 water vapor analyzers (with direct readout in kPa water vapor pressure, resolution 0.01 Pa) are used. For CO₂ analysis, two Sable Systems CA-10 CO₂ analyzers (resolution; 1 ppm CO₂) are used, while for O₂ analyzers a dual-channel O₂ analyzer (Sable Systems FC-2 Oxzilla; resolution 1 ppm O₂) is used. The barometric pressure analyzer inside the FC-2 O₂ analyzer resolves to 0.1 Pa (0.0001 kPa).

Sable System Data Acquisition and Processing

Data acquisition is performed using Sable Systems ExpeData software that employs a novel switching approach that permits constant, uninterrupted measurement of the incumbent airstream, while allowing frequent measurements of the incumbent airstream. In operation, the Sable system passes incumbent air from the chamber through both analyzer chains, but every ~15 min, switches the input of one of the analyzer chains so that it measures incumbent air instead for 3.5 min (Fig. A1). The analyzer measuring incumbent air is then switched back to measuring incumbent air. Both analyzer chains then continue to measure incumbent air, after which the input to the other analyzer chain is switched so that it measures incumbent air instead. After the measurement, the analyzer chain returns to measuring incumbent air. The cycle repeats, and although each analyzer chain is baselined (allowed to measure incumbent gas concentrations) multiple times per hour, at least one (and often both) of the analyzer chains is measuring incumbent gas concentrations at any given time. The switching control is also controlled during data acquisition using the Sable Systems Expedata software. All raw data are saved to a file for subsequent calculations.

During data analysis, the raw data are processed using Sable Systems ExpeData. The Sable system does not, at present, analyze data during acquisition. Every step in the process of data reduction is documented in an executable script that can be modified as desired. Briefly, the O₂ and CO₂ channels are corrected for water vapor dilution by multiplying them by BP/(BP – WVP), where BP is barometric pressure and WVP is water vapor pressure in equivalent units. The dried incumbent O₂ intervals (baselines) in each O₂ channel are then spanned to FIO₂ = 0.2094 using a Catmull-Rom splining technique (5), essentially eliminating analyzer drift. Delta channels are then created of (FICO₂ – FICO₂) and (FICO₂ – FICO₂), also using the multiple incumbent readings on both gases in conjunction with Catmull-Rom splining. The concurrent measurements from the two incumbent channels are averaged, and the concurrent sections of the two delta O₂ and two delta CO₂ channels are then matched and stitched together, thus creating a single delta O₂ and a single delta CO₂ channel, both of them drift corrected and without any interruptions from incumbent measurements. Flow rate is multiplied by (BP – WVP)/BP to remove the water vapor added by the subject to the incumbent flow. Standard equations (see below) are then used to calculate VCO₂ and VO₂. Sable Systems International has applied for a patent for the above-described background baselining technique.

Approximately every 2 wk, the Sable system CO₂ analyzers are calibrated with nitrogen (CO₂ zero) and CO₂ span gas (~1.0%), using the span gas manufacturer’s published gas concentrations without correction. The O₂ analyzer does not require spanning because this calibration is performed during data analysis, after correction for water vapor dilution, each time incumbent gas concentration is measured (see above). The water vapor pressure analyzers are calibrated during each run by switching a magnesium perchlorate desiccant column into the airstream while the incumbent airstream is selected. The dry air allows the water vapor pressure analyzer to be zeroed, and the increase in FICO₂ resulting from airstream desiccation allows water vapor pressure to be calculated (10) and is used to span the water vapor pressure analyzer automatically under ExpeData control. The system is validated ~ 1/mo using propane combustion, as described above.

The Sable system uses a conservative approach to response correction, modeled on first-order, gas-mixing kinetics as described elsewhere (3). It is applied after complete VO₂ and VCO₂ traces have been calculated. In essence, the first derivative of the trace is calculated, multiplied by a constant derived from the volume of the room and the volumetric flow rate, and added to the original data. Because of the long time constant of the room (~5 h), the multiplicative
constant is very large. Consequently, any significant noise in the derivatized data will overwhelm the original trace. A number of algorithms and approaches to low-noise derivatization exist (as do other approaches to response correction). After extensive testing, the following approach was adopted for the $V\dot{O}_2$ and $V\dot{CO}_2$ traces as the best compromise between low noise and speed of response. Briefly, starting at the beginning of the $V\dot{O}_2$ and $V\dot{CO}_2$ traces, successive half-hour sections of each trace (sampled at 1 Hz) were fitted by least squares fifth-degree polynomial regression. After each half-hour section was fitted, the resulting equation was utilized to calculate the best-fit prediction of the data over that section. The predicted values were added to a storage buffer. The section to be fitted was then shifted forward by 7.5 min, and the process was repeated until the end of the trace was reached. The mean of the summed predictions in the storage buffer was calculated, derivatized, and processed as described above.

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DISCLOSURES

John Lighton is the President of Sable Systems International.

REFERENCES